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LINE SIZE & PRESSURE DROP CALCULATION

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INPUT

Line Number		1	2	3	4	5	6	7
Drawing Ref		1	2	3	4	5	6	7
from						dic	E-214	P-2306
To		CR service	CASE - I			E-114	v-208	Unloading arm
Nominal or Internal diameter (N)		N	N	N	N	N	N	N
Diameter	[in]	2	4	4	10	0.75	1.5	18
Schedule (X for Standard) (Note 3)		X	X	X	X	X	X	X
Pipe roughness (X to default) (Note 1)	[in]	X	X	X	X	X	X	X
Phase (L, G, or M)		L	L	G	G	L	L	L
Liquid Flowrate	[gph]	6000	9084			185.2	185	1472000
Gas Flowrate	[gph]	0	0	692.7919746	692.7919746	0	0	0
Temperature	[°C]	40	32	32	32	150	150	80
Pressure	[psig]	10.00	0.00	4.50	4.50	3.1	2.5	0.1
Molecular Weight		71		28	28	133.5	133.5	0
Liquid Density	[g/m ³]	1580	986.4	0	0	826	826	820
Gas Density (X to calculate)	[g/m ³]	0	0	4.873	4.873	X	X	X
Cp/Cv (X to default 1)		0	0	X	X	X	1.2	1.2
Gas Compressibility Factor Z (X to default 1)		0	0	X	X	X	X	X
Gas Visc. (X to default 0.025)	[cP]	0	0	X	X	X	X	X
Liquid / Mixed Phase Viscosity	[cP]	0.393	641.160			1.6	2	0
Liquid Surface Tension	[dynes/cm]					20.2	0	0

FORMAL PROCESS DATA ANALYSIS LIQUID-OK LIQUID-OK GAS-OK GAS-OK LIQUID-OK LIQUID-OK Mixing Liquid

Excel Spreadsheets Chemical Engineering

**Richard Smith, Hiroshi Inomata, Cor
Peters**



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