

Table 3 Suction, Discharge, and Liquid Line Capacities in Tons for Refrigerant 22 (Single- or High-Stage Applications)

Line Size Type L Copper, O.D.		Suction Lines ($\Delta t = 2^\circ\text{F}$)				Discharge Lines ($\Delta t = 1^\circ\text{F}$, $\Delta p = 3.05$ psf)		Line Size Type L Copper, O.D.	Liquid Lines See notes a and b		
		-40	-20	0	20	Saturated Suction Temperature, $^\circ\text{F}$			Type L Copper, O.D.	Vert. = 100 ft 1800 ft	$\Delta t = 1^\circ\text{F}$ $\Delta p = 3.05$
		Corresponding Δp , psi/100 ft				-40	40				
1/2	—	—	—	—	0.40	0.75	0.85	1/2	2.5	3.6	
5/8	—	0.32	0.51	0.76	1.1	1.4	1.6	5/8	3.7	6.7	
7/8	0.52	0.86	1.3	2.0	2.9	3.7	4.2	7/8	7.6	18.2	
1 1/8	1.1	1.7	2.7	4.0	5.8	7.5	8.5	1 1/8	13.2	37.0	
1 3/8	1.9	3.1	4.7	7.0	10.1	13.1	14.8	1 3/8	20.2	64.7	
1 5/8	3.0	4.8	7.4	11.1	16.0	20.7	23.4	1 5/8	28.5	102.5	
2 1/8	4.7	7.6	11.6	17.1	25.1	32.6	36.5	2 1/8	49.6	213.0	
2 3/8	7.0	11.0	17.0	25.0	36.0	46.0	51.4	2 3/8	76.5	376.9	
3 1/8	11.5	18.4	28.0	44.0	65.0	82.0	92.9	3 1/8	109.2	601.5	
3 3/8	16.0	25.3	38.4	58.0	86.0	109.0	124.4	3 3/8	147.8	895.7	
4 1/8	24.8	39.6	59.2	88.0	130.0	166.0	188.4	4 1/8	232.1	1263.2	
Steel								Steel			
IPS	SC&H							IPS	SC&H		
1/2	40	—	0.58	0.58	0.83	1.5	1.7	1/2	800	3.8	5.7
3/4	40	0.50	0.8	1.2	1.8	3.3	3.7	3/4	800	6.9	12.8
1	40	0.95	1.5	2.3	3.4	6.1	6.9	1	800	11.5	25.2
1 1/4	40	2.0	3.2	4.8	7.0	12.6	14.3	1 1/4	800	20.6	54.1
1 1/2	40	3.0	4.7	7.2	10.5	19.0	21.5	1 1/2	800	28.3	82.6
2	40	5.7	9.1	13.9	20.2	36.6	41.4	2	400	53.8	192.0
2 1/2	40	9.2	14.6	22.1	32.2	58.1	65.9	2 1/2	400	78.7	305.8
3	40	14.2	23.7	36.0	54.8	102.8	116.4	3	400	118.5	540.3
4	40	23.1	37.5	56.8	85.0	169.5	197.3	4	400	204.2	1001.2

Notes:
 1. Table capacities are in tons of refrigeration.
 Δp = pressure drop from line friction, psi per 100 ft of equivalent line length
 Δt = corresponding change in saturation temperature, $^\circ\text{F}$ per 100 ft
 2. Line capacity for other saturation temperatures Δt and equivalent lengths L_e

$$\text{Line capacity} = \text{Table capacity} \left(\frac{\text{Table } L_e}{\text{Actual } L_e} + \frac{\text{Actual } \Delta t}{\text{Table } \Delta t} \right)^{1.8}$$

 3. Saturation temperature Δt for other capacities and equivalent lengths L_e

$$\Delta t = \text{Table } \Delta t \left(\frac{\text{Actual } L_e}{\text{Table } L_e} \right) \left(\frac{\text{Actual capacity}}{\text{Table capacity}} \right)^{1.8}$$

*Using shown is recommended where any gas generated in receiver must return up condenser line to condenser without reversing condenser flow. Water-cooled condensers, where receiver ambient temperature may be higher than refrigerant condensing temperature, fall into this category.

4. Values based on 105 $^\circ\text{F}$ condensing temperature. Multiply table capacities by the following factors for other condensing temperatures.

Condensing Temperature, $^\circ\text{F}$	Suction Line	Discharge Line
80	1.11	0.79
90	1.07	0.88
100	1.03	0.95
110	0.97	1.04
120	0.90	1.10
130	0.84	1.18
140	0.80	1.26

*Line pressure drop Δp is conservative, if subcooling is substantial or line is short, a smaller size line may be used. Applications with very little subcooling on very long lines may require a larger line.

Table 4 Suction, Discharge, and Liquid Line Capacities in Tons for Refrigerant 22 (Intermediate- or Low-Stage Duty)

Line Size Type L Copper, O.D.		Suction Lines ($\Delta t = 2^\circ\text{F}$) ^a					Discharge Lines ($\Delta t = 2^\circ\text{F}$) ^a	Liquid Lines	
		Saturated Suction Temperature, $^\circ\text{F}$							
		-90	-80	-70	-60	-50	-40	-30	
5/8	—	—	—	—	—	—	—	—	
7/8	—	0.18	0.25	0.34	0.46	0.61	0.79	1.0	0.7
1 1/8	—	0.26	0.31	0.39	0.54	0.72	1.0	2.1	3.8
1 3/8	—	0.6	0.9	1.2	1.6	2.2	2.8	3.6	6.6
1 5/8	—	1.0	1.4	1.9	2.6	3.4	4.3	5.7	10.5
2 1/8	—	2.1	3.0	4.1	5.5	7.2	9.3	11.9	21.7
2 3/8	—	3.8	5.3	7.2	9.7	12.7	16.5	21.1	38.4
3 1/8	—	6.1	8.5	11.6	15.5	20.4	26.4	33.8	61.4
3 3/8	—	9.1	12.7	17.3	23.1	30.4	39.4	50.2	91.2
4 1/8	—	12.9	18.0	24.3	32.7	43.0	55.6	70.9	128.6
5 1/8	—	20.2	27.3	36.9	49.9	65.1	84.8	108.9	209.5
6 1/8	—	31.5	42.1	56.9	76.6	100.5	130.4	169.4	349.4

Notes:
 1. Table capacities are in tons of refrigeration.
 Δp = pressure drop from line friction, psi per 100 ft of equivalent line length
 Δt = corresponding change in saturation temperature, $^\circ\text{F}$ per 100 ft
 2. Line capacity for other saturation temperatures Δt and equivalent lengths L_e

$$\text{Line capacity} = \text{Table capacity} \left(\frac{\text{Table } L_e}{\text{Actual } L_e} + \frac{\text{Actual } \Delta t}{\text{Table } \Delta t} \right)^{1.8}$$

 3. Saturation temperature Δt for other capacities and equivalent lengths L_e

$$\Delta t = \text{Table } \Delta t \left(\frac{\text{Actual } L_e}{\text{Table } L_e} \right) \left(\frac{\text{Actual capacity}}{\text{Table capacity}} \right)^{1.8}$$

 4. Refer to refrigerant thermodynamic property tables (Chapter 20 of the 2013 ASHRAE Handbook—Fundamentals) for pressure drop corresponding to Δt .

^aSee section on Pressure Drop Considerations.

5. Values based on 0 $^\circ\text{F}$ condensing temperature. Multiply table capacities by the following factors for other condensing temperatures. Flow rates for discharge lines are based on -50 $^\circ\text{F}$ evaporating temperature.

Condensing Temperature, $^\circ\text{F}$	Suction Line	Discharge Line
-30	1.09	0.58
-20	1.06	0.71
-10	1.03	0.83
0	1.00	1.00
10	0.97	1.20
20	0.94	1.43
30	0.90	1.80

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reactions answer key after trading partners the balanced equation is $\text{ce nacn left aq right ce hbr left aq right rightarrow ce}$
 $\text{nabr left aq right ce hcn left g right}$ think about your result

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