

Table 3 Suction, Discharge, and Liquid Line Capacities in Tons for Refrigerant 22 (Single- or High-Stage Applications)

Line Size Type L Copper, CDD		Suction Lines ($\Delta t = 2^\circ\text{F}$)				Discharge Lines ($\Delta t = 1^\circ\text{F}$, $\Delta p = 3.05$ psf)		Line Size Type L Copper, CDD	Liquid Lines See notes a and b		
		-40	-20	0	20	40	Saturated Suction Temperatures, $^\circ\text{F}$		Type L Copper, CDD	Visc. = 100 cP 1000 gpm	$\Delta t = 1^\circ\text{F}$ $\Delta p = 3.05$
Corresponding Δp , psi/100 ft		1.15	1.6	2.22	2.91	-40	-40				
1/2	—	—	—	0.40	0.6	0.75	0.85	1/2	2.5	3.6	
5/8	—	0.32	0.51	0.76	1.1	1.4	1.6	5/8	3.7	6.7	
7/8	0.52	0.66	1.3	2.0	2.9	3.7	4.2	7/8	7.6	18.2	
1 1/8	1.1	1.7	2.7	4.0	5.8	7.5	8.5	1 1/8	13.2	37.0	
1 3/8	1.9	3.1	4.7	7.0	10.1	13.1	14.8	1 3/8	20.2	64.7	
1 5/8	3.0	4.8	7.4	11.1	16.0	20.7	23.4	1 5/8	28.5	88.2	
2 1/8	4.2	6.6	10.0	14.5	21.1	27.6	31.1	2 1/8	49.6	133.0	
2 3/8	6.7	10.0	15.0	22.0	32.1	41.4	46.4	2 3/8	76.5	216.0	
2 5/8	10.0	15.0	22.0	32.1	46.4	60.8	68.3	3 1/8	109.2	301.5	
3 1/8	17.5	26.4	44.0	65.0	92.9	120.2	136.2	3 5/8	147.8	405.7	
3 3/8	26.0	42.3	65.4	96.6	137.8	178.4	202.1	4 1/8	192.1	523.2	
4 1/8	36.8	59.6	92.2	136.3	194.3	251.1	284.4				
Steel								Steel			
IPS	SCH					IPS	SCH				
1/2	40	—	0.58	0.58	0.83	1.2	1.5	1/2	800	3.8	5.7
3/4	40	0.50	0.8	1.2	1.8	2.5	3.3	3/4	800	6.9	12.8
1	40	0.95	1.5	2.3	3.4	4.8	6.1	1	800	11.5	21.2
1 1/4	40	2.0	3.2	4.8	7.0	9.9	12.6	1 1/4	800	20.6	34.1
1 1/2	40	3.0	4.7	7.2	10.5	14.8	19.0	1 1/2	800	28.3	47.6
2	40	5.7	9.1	13.9	20.2	28.5	36.8	2	400	53.8	92.0
2 1/2	40	9.2	14.6	22.1	32.2	45.4	58.1	2 1/2	400	78.7	130.8
3	40	14.2	23.7	36.0	56.8	80.1	102.8	3	400	118.5	190.3
4	40	23.1	37.5	56.8	83.1	115.9	148.2	4	400	204.2	331.2

- Notes:
 1. Table capacities are in tons of refrigeration.
 Δp = pressure drop from line friction, psi per 100 ft of equivalent line length
 Δt = corresponding change in saturation temperature, $^\circ\text{F}$ per 100 ft
 2. Line capacity for other saturation temperatures Δt and equivalent lengths L_e

$$\text{Line capacity} = \text{Table capacity} \left(\frac{\text{Table } L_e}{\text{Actual } L_e} + \frac{\text{Actual } \Delta t}{\text{Table } \Delta t} \right)^{1.8}$$

 3. Saturation temperature Δt for other capacities and equivalent lengths L_e

$$\Delta t = \text{Table } \Delta t \left(\frac{\text{Actual } L_e}{\text{Table } L_e} \right) \left(\frac{\text{Actual capacity}}{\text{Table capacity}} \right)^{1.8}$$

*Using shown is recommended where any gas generated in receiver must return up condenser line to condenser without reversing condenser flow. Water-cooled condensers, where receiver ambient temperature may be higher than refrigerant condensing temperature, fall into this category.

4. Values based on 105 $^\circ\text{F}$ condensing temperature. Multiply table capacities by the following factors for other condensing temperatures.

Condensing Temperature, $^\circ\text{F}$	Suction Line	Discharge Line
80	1.11	0.79
90	1.07	0.88
100	1.03	0.95
110	0.97	1.04
120	0.90	1.10
130	0.84	1.18
140	0.80	1.26

*Line pressure drop Δp is conservative, if subcooling is substantial or line is short, a smaller size line may be used. Applications with very little subcooling on very long lines may require a larger line.

Table 4 Suction, Discharge, and Liquid Line Capacities in Tons for Refrigerant 22 (Intermediate- or Low-Stage Duty)

Line Size Type L Copper, O/D		Suction Lines ($\Delta t = 2^\circ\text{F}$) ^a					Discharge Lines ($\Delta t = 2^\circ\text{F}$) ^a	Liquid Lines	
		Saturated Suction Temperature, $^\circ\text{F}$							
		-90	-80	-70	-60	-50	-40	-30	
5/8	—	—	—	—	—	—	—	—	0.7
7/8	—	0.18	0.25	0.34	0.46	0.61	0.79	1.0	1.9
1 1/8	—	0.26	0.31	0.39	0.54	1.2	1.6	2.1	3.8
1 3/8	—	0.6	0.9	1.2	1.6	2.2	2.8	3.6	6.6
1 5/8	—	1.0	1.4	1.9	2.6	3.4	4.2	5.7	10.5
2 1/8	—	2.1	3.0	4.1	5.5	7.2	9.3	11.9	21.7
2 3/8	—	3.8	5.3	7.2	9.7	12.7	16.5	21.1	38.4
2 5/8	—	6.1	8.5	11.6	15.5	20.4	26.4	33.8	61.4
3 1/8	—	9.1	12.7	17.3	23.1	30.4	39.4	50.2	91.2
4 1/8	—	12.9	18.0	24.3	32.7	43.0	55.6	70.9	128.6
5 1/8	—	20.2	27.3	36.9	49.8	65.1	83.8	107.5	200.5
6 1/8	—	37.5	52.1	71.0	94.6	124.2	160.5	204.2	369.4

- Notes:
 1. Table capacities are in tons of refrigeration.
 Δp = pressure drop from line friction, psi per 100 ft of equivalent line length
 Δt = corresponding change in saturation temperature, $^\circ\text{F}$ per 100 ft
 2. Line capacity for other saturation temperatures Δt and equivalent lengths L_e

$$\text{Line capacity} = \text{Table capacity} \left(\frac{\text{Table } L_e}{\text{Actual } L_e} + \frac{\text{Actual } \Delta t}{\text{Table } \Delta t} \right)^{1.8}$$

 3. Saturation temperature Δt for other capacities and equivalent lengths L_e

$$\Delta t = \text{Table } \Delta t \left(\frac{\text{Actual } L_e}{\text{Table } L_e} \right) \left(\frac{\text{Actual capacity}}{\text{Table capacity}} \right)^{1.8}$$

 4. Refer to refrigerant thermodynamic property tables (Chapter 20 of the 2013 ASHRAE Handbook—Fundamentals) for pressure drop corresponding to Δt .
 5. See section on Pressure Drop Considerations.

5. Values based on 0 $^\circ\text{F}$ condensing temperature. Multiply table capacities by the following factors for other condensing temperatures. Flow rates for discharge lines are based on -50 $^\circ\text{F}$ evaporating temperature.

Condensing Temperature, $^\circ\text{F}$	Suction Line	Discharge Line
-30	1.09	0.58
-20	1.06	0.71
-10	1.03	0.83
0	1.00	1.00
10	0.97	1.20
20	0.94	1.43
30	0.90	1.80

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